



Development of a Molten-salt Thermocline Thermal Storage System for Parabolic Trough Plants

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Need for Thermal Storage for Trough Plants

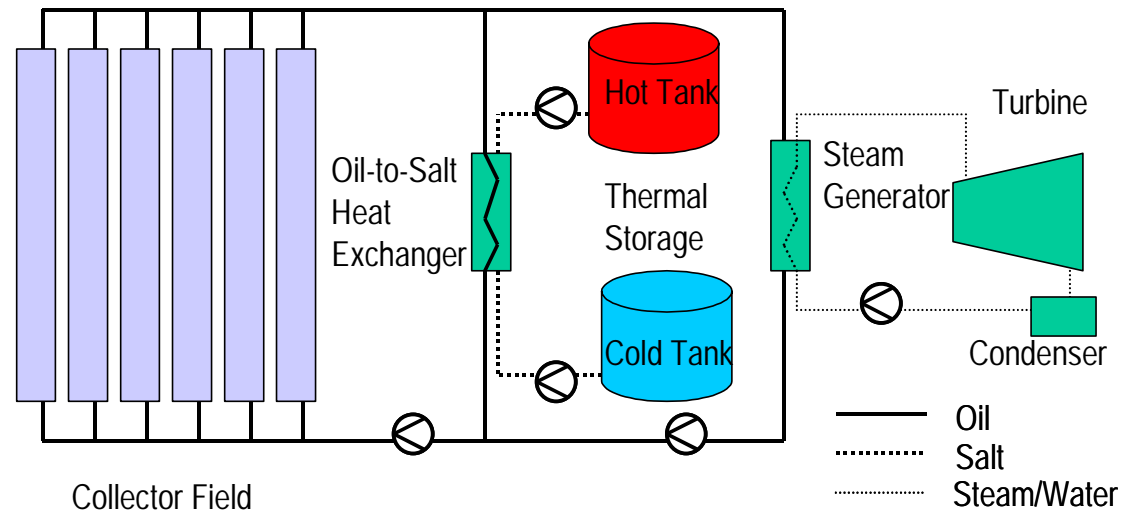
- Enables dispatchability without fossil fuel
- Provides load shifting
- Increases revenue from plants
- Allows higher solar fraction in combined cycle (CC) plants
- Improves economics of solar in CC plants
- Decouples collection from electricity production

How Thermal Storage Can be Integrated into a Solar Plant

- Direct
 - Heat transfer fluid is the **same** as the storage media
 - Examples: SEGS 1 (mineral oil), Solar Two (molten salt)
- Indirect
 - Heat transfer fluid is transferred to **another** media
 - Examples: SEGS plant (synthetic oil transfers heat to molten salt in a two tank system).

Estimated Capital Cost
Of a Two-Tank Molten Salt
System: **\$31/kWh_t**

Long-term Goal: **\$10/kWh_t**



Objective of Thermocline Development Project

- *Reduce the capital costs of storage for parabolic trough plants relative to the baseline (indirect two-tank molten-salt system).*
- *Address the technical risks associated with thermocline storage:*
 - *Compatibility of filler materials with molten-salt*
 - *Unproven concept*
 - *Safety issues of fuel (Therminol) next to oxidizer (nitrate salt)*



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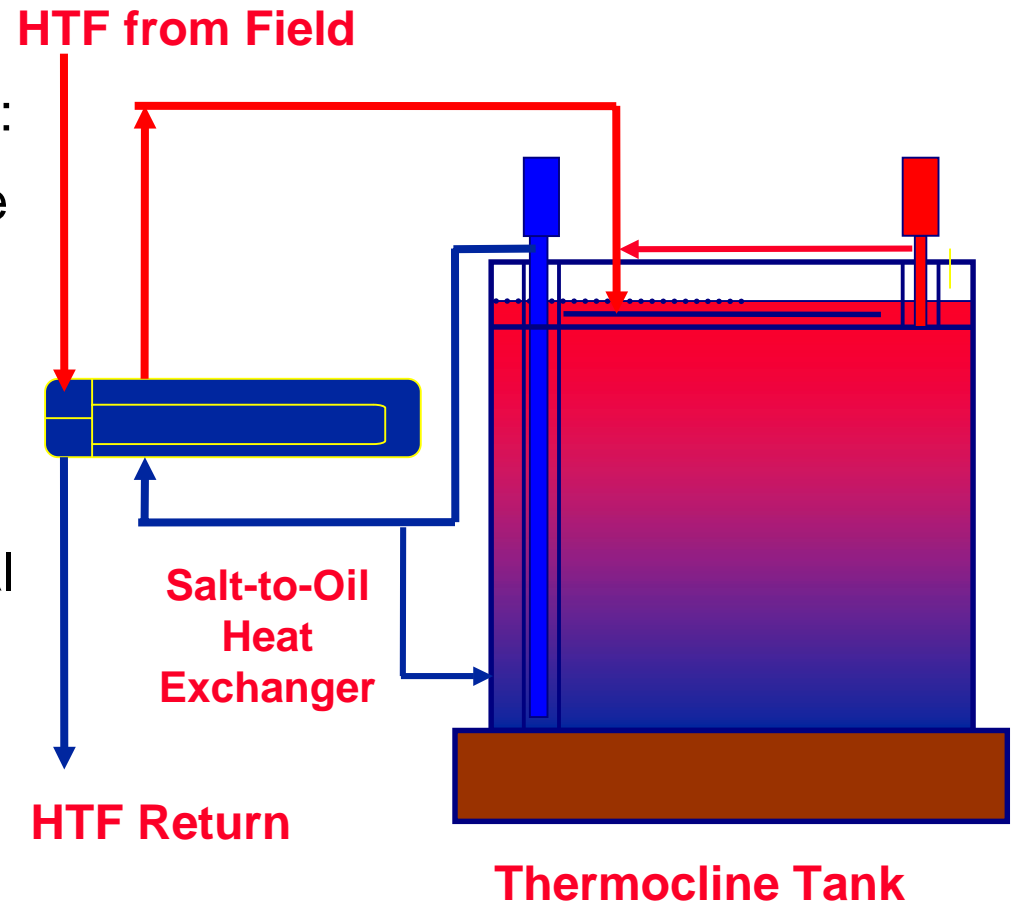
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Description of Thermocline System

A thermocline molten salt system:

- Uses a single tank to storage energy
- Has a thermal gradient that separates the hot from cold fluid.
- Uses a low-cost filler material to displace higher-cost molten nitrate salt.



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Development Activity Divided into 3 Areas

- Model thermocline system: Simulate performance and economics
- Evaluate candidate filler materials: Isothermal and thermal cycling tests
- Test a small pilot-scale thermocline: 2.3 MWh capacity to validate performance and operating characteristics

Modeling a Thermocline System

- Transient thermal behavior simulated by the Schumann equations which describe the heat transfer between a fluid and a packed bed.
- Finite difference representation of these equations enabled calculations of the thermal gradient and inlet and outlet temperatures as a function of time.
- Also enabled calculation of extracted energy and capacity.

$$(\rho C_p)_f \varepsilon \frac{\partial T_f}{\partial \tau} = -\frac{(m C_p)_f}{A} \frac{\partial T_f}{\partial y} + h_v (T_b - T_f)$$

$$(\rho C_p)_b (1 - \varepsilon) \frac{\partial T_b}{\partial \tau} = h_v (T_f - T_b)$$



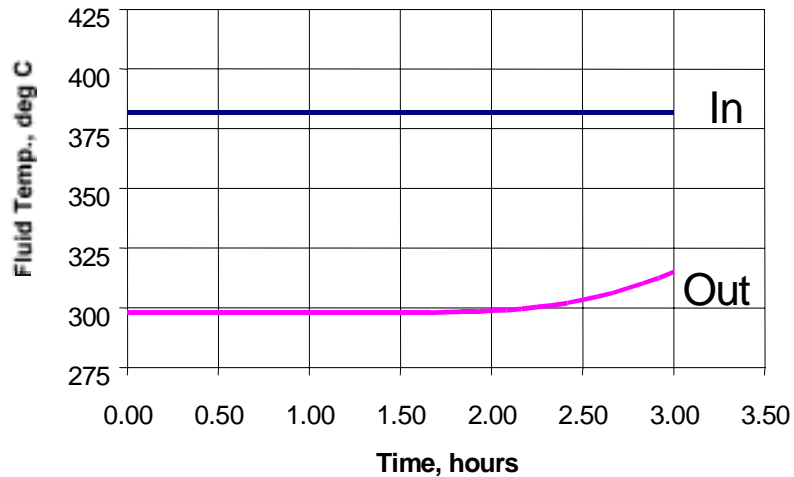
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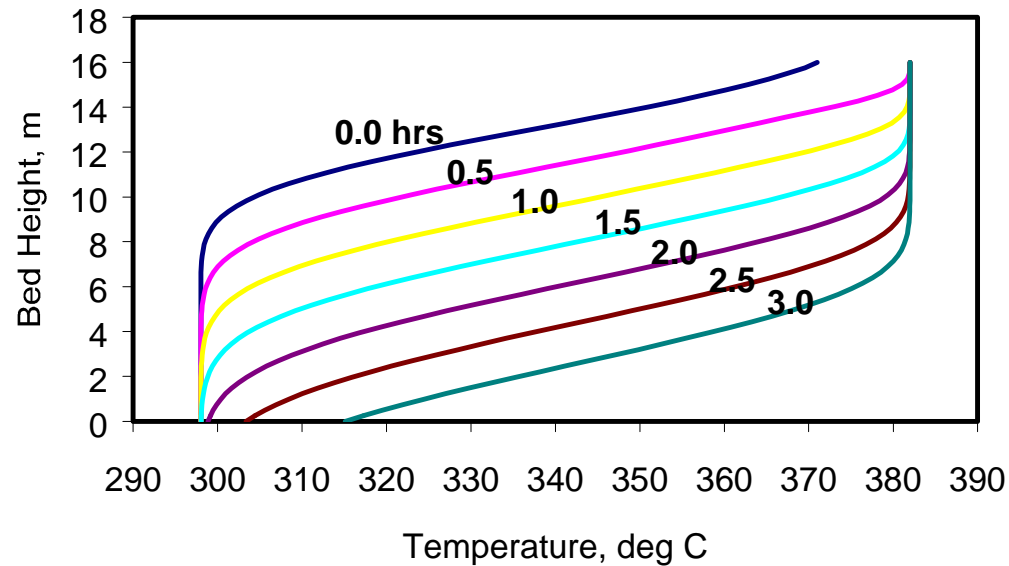
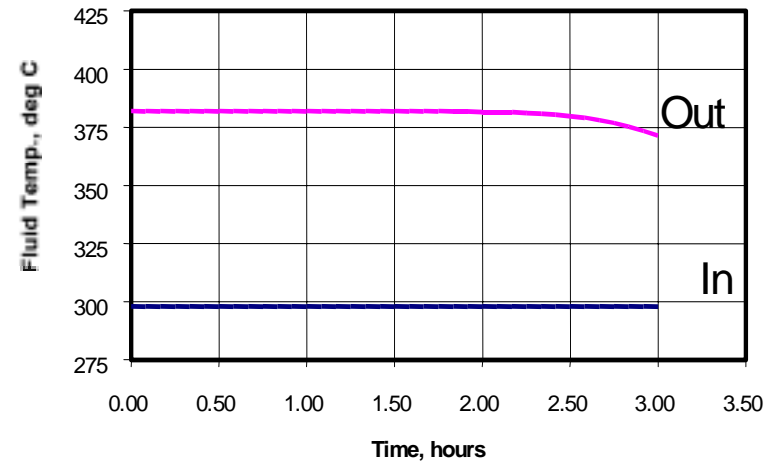
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Model Results

Charging



Discharging



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Thermal Gradient During Charging

Screening Potential Filler Materials in Nitrate Salt

- Seventeen commonly mined minerals and crushed rock were evaluated for their compatibility with nitrate salts
- The ideal filler material would have the following properties:
 - Inexpensive
 - Widely available
 - Low void fraction
 - Compatible with nitrate salts
 - Have a high heat capacitance

Chemical Name	Mineral Name	Chemical Formula
Aluminum oxide	Corundum	Al_2O_3
Aluminum oxyhydroxide	Bauxite*	$\text{AlO}_x(\text{OH})_z$
Barium carbonate	Witherite	BaCO_3
Barium sulfate	Barite	BaSO_4
Calcium carbonate	Marble	CaCO_3
Calcium fluoride	Fluorite	CaF_2
Calcium sulfate	Anhydrite	CaSO_4
Iron (II,III) oxides	Taconite	$\text{Fe}_2\text{O}_3, \text{Fe}_3\text{O}_4$
Iron titanate	Ilmenite	FeTiO_3
Magnesium carbonate	Magnesite	MgCO_3
Silicon carbide	Carborundum	SiC
Tin oxide	Cassiterite	SnO_2
Calcium hydroxyphosphate	Hydroxylapatite	$\text{Ca}_5(\text{PO}_4)_3 \text{OH}$
Calcium fluorphosphate	Fluorapatite	$\text{Ca}_5(\text{PO}_4)_3\text{F}$
Calcium carbonate	Limestone	$\text{CaCO}_3 \bullet \text{H}_2\text{O}$
Silicon dioxide	Quartzite	SiO_2



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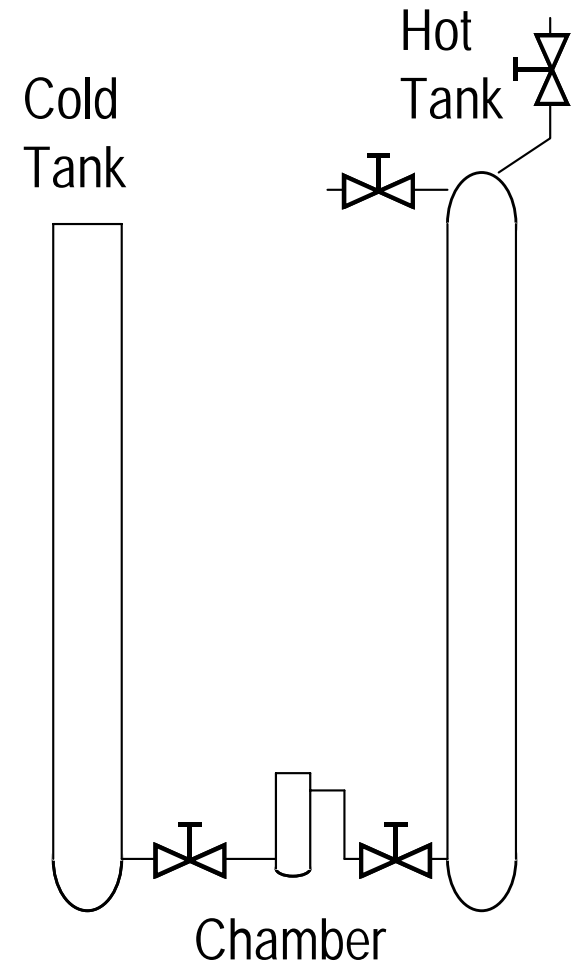
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Isothermal Tests of Filler Materials

- Evaluated candidate materials in nitrate salts at 400 C. Samples were removed at 10, 100, 400 and 1000 hours of exposure.
- Samples were washed, weighed, and photographed. The salt was analyzed for contaminants.
- Results indicated the most promising materials were: quartzite, taconite, marble, NM limestone, apatite, corundum, scheelite, and cassiterite.

Thermal Cycling Tests

- Evaluated how well materials held up to thermal cycling condition expected in a thermocline system. At least 350 cycles between 290 and 400 deg C were conducted on each sample.
- Samples tested: taconite, marble, NM limestone, quartzite, and silica sand.
- Results:
 - NM Limestone fell apart
 - Marble softened and individual grains appeared to enlarge
 - Taconite pellets held together well. Absorbed some salt in pores
 - Quartzite rock and silica sand held up remarkable well and were selected as filler material for pilot-scale test



Thermal Cycling System



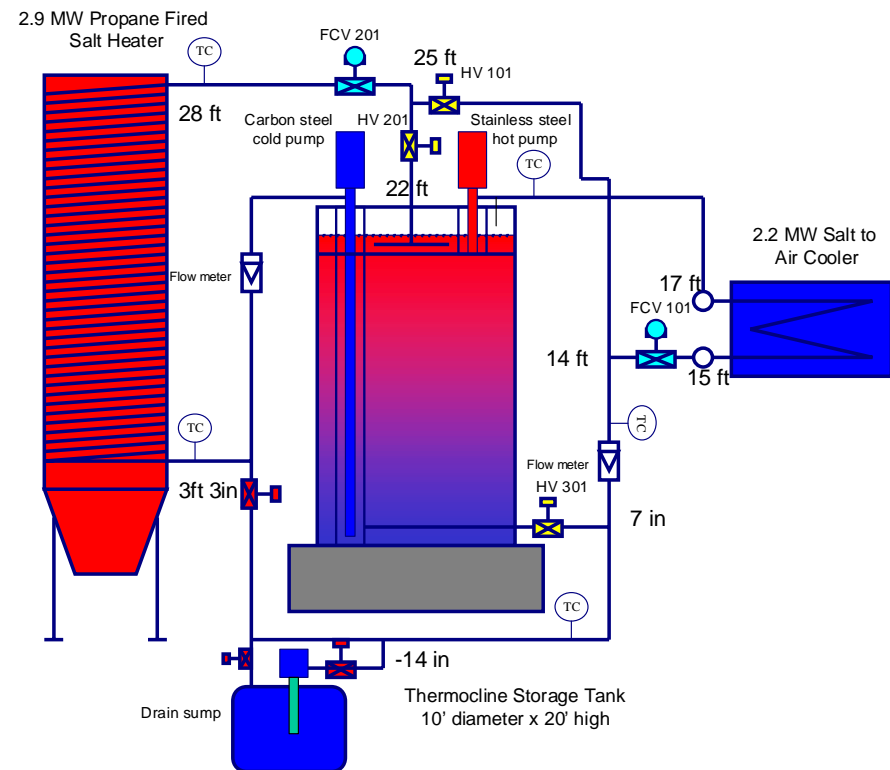
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Thermocline Test

- Evaluate on a larger (pilot-scale) a molten-salt thermocline concept.
- Fabricated a 6 m tall by 3 m diameter carbon steel tank. Filled tank with a 2:1 mixture of quartzite rock and silica sand to a level of 5.2 m.
- Sodium nitrate and potassium nitrate were melted and added to tank.
- A propane heater simulated the heat input from the solar field (via the salt-to-oil heat exchanger).
- A forced-air cooler simulated heat rejection to the steam generator (through the salt-to-oil exchanger).



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Tests Conducted

- Verification of heat capacity of system
- Evaluation of size and shape of thermal gradient
- Evaluation of change of shape of gradient over time
- Measurement of heat loss over time



Pilot-Scale Thermocline System



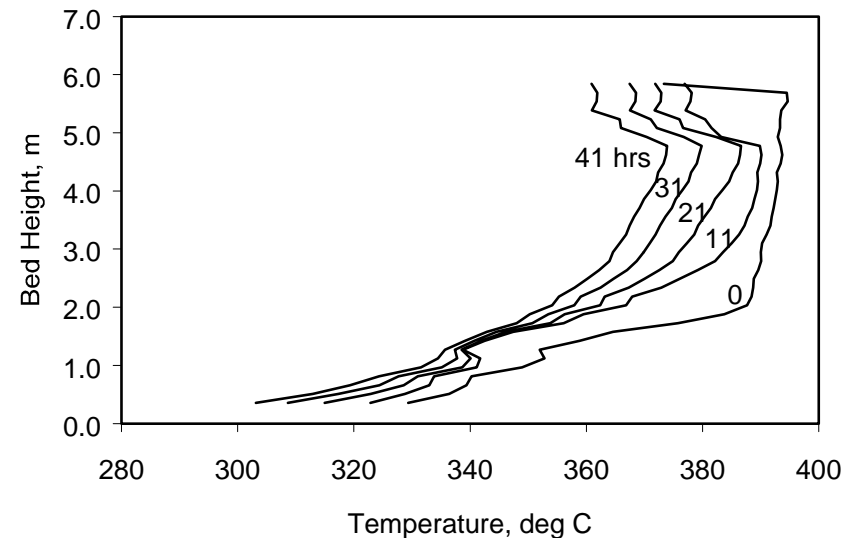
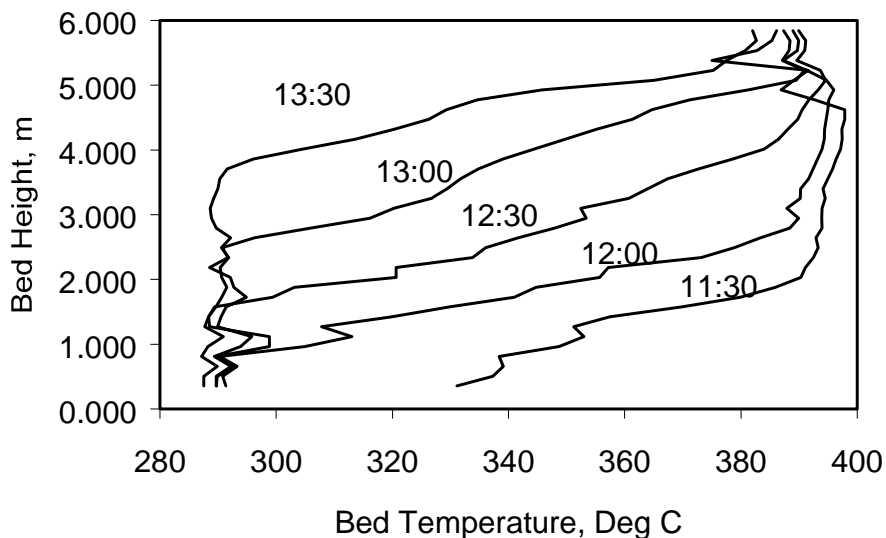
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Thermocline Test Results

- Capacity measured to be 2.44 MWh (slightly higher than 2.3 MWh design estimate.)
- Height of gradient during charging matches modeled profile.
- Gradient tended to become more tapered after 41 hours, but can still yield useful energy at a reasonable temperature potential.
- Heat loss was higher than modeled (likely due to heat loss through pump penetrations at the top (which weren't modeled.)



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Profile during discharging and stagnant with heat loss

Economic Analysis for a 688 MWh_t Two-tank and Thermocline Systems

Component	Two-Tank Molten Salt	Thermocline with Quartzite
Nitrate Solar Salt, \$k	11800	3800
Filler Material, \$k	0	2200
Tank(s), \$k	3800	2400
Salt-to-oil Heat Exchanger, \$k	5500	5500
Total, \$k	21100	13900
Specific Cost, \$/kWh	31	20

*Thermocline Molten-Salt System is 65% the cost of a
Two-tank Molten-Salt System*



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Summary

- A molten salt thermocline system has been developed that is lower cost than a two-tank molten salt system.
- Isothermal and thermal cycling tests showed that silica sand and quartzite rock as well as taconite were compatible with nitrate salts.
- The feasibility of a molten-salt thermocline system was proven on a pilot scale 2.3 MWh storage system.